

2

2

10

1:

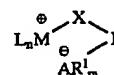
- 24

30

3:

65

(D)

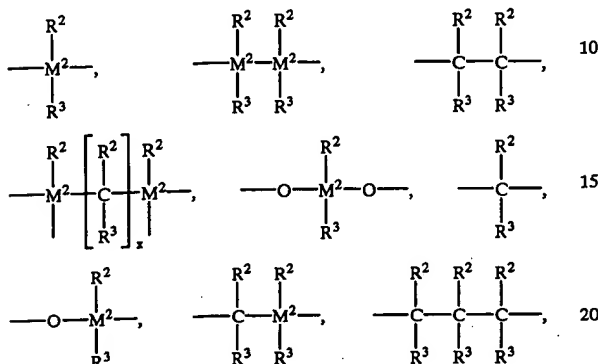


For the purposes of the present invention, an electron donor is an atom of group IVa, Va, VIa or VIIa of the

Periodic Table of the Elements, which can bear substituents such as C_1-C_{20} -hydrocarbon groups. Preference is given to O, NR^4 , NR^4 , NR^4 , PR^4 , PR^4 , PR^4 , $P(OR^4)_2$, $P(OR^4)_2$ or Cl, where R^4 is C_1-C_{20} -alkyl or C_6-C_{14} -aryl.

Two radicals L can be linked to one another via a bridge (Z).

The bridge Z is preferably



$=BR_2$, $-AIR^2$, $-Ge-$, $-O-$, $-S-$, $=SO$, $=SO_2$, $-NR_2$, $=CO$, $=PR^2$ or $=P(O)R^2$, where R^2 and R^3 are identical or different and are each a hydrogen atom, a halogen atom, a C_1-C_{20} -alkyl group, a C_1-C_1 -fluoroalkyl group, a C_1-C_{10} -alkoxy group, a C_6-C_{14} -aryl group, a C_6-C_{10} -fluoroaryl group, a C_6-C_{10} -aryloxy group, a C_2-C_{10} -alkenyl group, a C_7-C_{40} -arylalkyl group, a C_7-C_{40} -alkylaryl group, a C_8-C_{40} -arylalkenyl group and x is a number from zero to 18, or R^2 and R^3 together with the atoms-connecting them form one or more rings and R^2 or/and R^3 can be bonded to L and M^2 is silicon, germanium or tin.

Z can also link two or more identical or different groups $L_nM^*XBA-R^1_m$ with one another.

For the purposes of the present invention, a heteroatom is any atom of the Periodic Table of the Elements with the exceptions of carbon and hydrogen. Preference is given to O, S and N.

Hydrocarbon groups X and B can be saturated or unsaturated, linear or branched, eg. a C_1-C_{20} -alkyl group, a C_6-C_{14} -aryl group, a C_2-C_{10} -alkenyl group, a C_7-C_{40} -arylalkyl group, a C_7-C_{40} -alkylaryl group or a C_8-C_{40} -arylalkenyl group. Preference is given to substituted or unsubstituted alkyl groups which can also have aromatic structural elements.

Preference is given to n=1 when M is an element of group IIb of the Periodic Table of the Elements; n=2 when M is a metal atom of group IVb of the Periodic Table of the Elements; n=3 when M is an element of group Vb of the Periodic Table of the Elements; and n=4 when M is an element of group VIb of the Periodic Table of the Elements.

R^1 is a C_1-C_{40} -hydrocarbon radical which is perhalogenated with halogen such as fluorine, chlorine, bromine or iodine, in particular a perhalogenated C_1-C_{30} -alkyl group such as trifluoromethyl, pentachloroethyl, heptafluoroisopropyl, or monofluoroisobutyl or a perhalogenated C_6-C_{30} -aryl group such as pentafluorophenyl, heptachloronaphthyl, heptafluoronaphthyl or heptafluorotolyl.

Particular preference is given to compounds of the formula 1, where

M is a metal atom of group IVb of the Periodic Table of the Elements, such as titanium, zirconium or hafnium, n is equal to 2,

L are identical or different and are each a substituted or unsubstituted cyclopentadienyl group, where two radicals L can be linked to one another via a bridge Z and Z is CR^2R^3 or SiR^2R^3 or a unit $Si-(CR^2R^3)_x-Si$ which links two fragments $L_nM^*XBA-R^1_m$ with one another, where x is an integer from 0 to 10, preferably x=6,

X and B together form a three-membered to five-membered (C_3-C_5)-alkyl chain which is saturated or unsaturated and can be substituted by C_1-C_{20} -hydrocarbon radicals,

A is a metal of group Ib, IIb, IIIa, IVa, Va, Vb of the Periodic Table of the Elements,

R^1 are identical or different and are each a perfluorinated alkyl or aryl group having from 1 to 20 carbon atoms and

m is equal to 2, 3 or 4.

Very particular preference is given to compounds of the formula 1, where

M is zirconium,

n is equal to 2,

L are identical or different and are each a substituted cyclopentadienyl group, where two radicals L are bonded to one another via a bridge Z, where Z is CR^2R^3 or SiR^2R^3 ,

X and B together form an unsaturated four-membered (C_4)-alkyl chain whose hydrogen atoms can also be replaced by C_1-C_{20} -alkyl groups,

A is a boron atom,

R^1 are identical and are each a pentafluorophenyl group (C_6F_5) and

m is equal to 3.

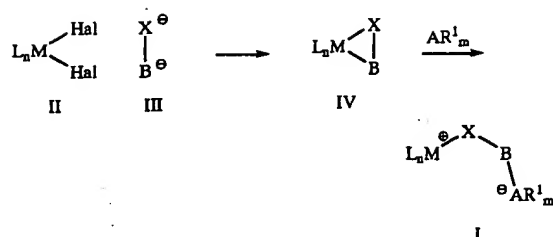
Examples of compounds of the invention are:

- 35 bis(cyclopentadienyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- bis(methylcyclopentadienyl)Zr⁺C₂CHCHCH₂B⁻(C₆F₅)₃;
- bis(n-butylcyclopentadienyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- bisindenylZr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- (tert-butylamido)dimethyl(tetramethyl-η⁵-cyclopentadienyl)silaneZr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- bis(2-methylbenzoindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- dimethylsilanediybis(2-methylindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- dimethylsilanediybisindenylZr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- 45 dimethylsilanediybis(2-methylbenzoindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- dimethylsilanediybis(2-methylindenyl)(2-methylbenzoindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- dimethylsilanediybis(2-methylbenzoindenyl)(2-methyl-4-phenylindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- dimethylsilanediybis(2-methylindenyl)(4-phenylindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- dimethylsilanediybis(2-methyl-4-phenylindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- 55 dimethylsilanediybis(2-methyl-4,6-diisopropylindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- dimethylsilanediybis(2-methyl-4-naphthylindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- isopropylidene(cyclopentadienyl)(fluorenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- 60 isopropylidene(cyclopentadienyl)(indenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- [4-η⁵-cyclopentadienyl-4,7,7-trimethyl-(η⁵-4,5,6,7-tetrahydroindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃;
- dimethylsilanediybis(2-methylindenyl)Zr⁺OCH₂CH₂CH₂B⁻(C₆F₅)₃;
- dimethylsilanediybisindenylZr⁺OCH₂CH₂CH₂B⁻(C₆F₅)₃;

phenylmethylsilanediyldiyl(2-methylindenyl)(4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
phenylmethylsilanediyldiylbis(2-methyl-4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
phenylmethylsilanediyldiylbis(2-ethyl-4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
phenylmethylsilanediyldiylbis(2-methyl-4,6-diisopropylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
phenylmethylsilanediyldiylbis(2-methyl-4-naphthylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylenebis(2-methylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylenebisindenyl $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylenebis(2-methyl-4,5-benzoidindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylene(2-methyl-4,5-benzoidindenyl)(2-methylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylene(2-methyl-4,5-benzoidindenyl)(2-methyl-4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylene(2-methylindenyl)(4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylenebis(2-methyl-4,5-benzoidindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylenebis(2-methyl-4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylenebis(2-methyl-4,6-diisopropylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylenebis(2-methyl-4-naphthylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylenebis(2-ethyl-4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylenebis(2-ethyl-4,6-diisopropylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
ethylenebis(2-ethyl-4-naphthylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
dimethylsilanediyldiylbis(2-ethyl-4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
dimethylsilanediyldiylbis(2,3,5-trimethylcyclopentadienyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$;
1,6-{bis[methylsilyl]bis(2-methyl-4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$ }hexane;
1,6-{bis[methylsilyl]bis(2-ethyl-4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$ }hexane;
1,6-{bis[methylsilyl]bis(2-methyl-4-naphthylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$ }hexane;
1,6-{bis[methylsilyl]bis(2-methyl-4,5-benzoidindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$ }hexane;
1,6-{bis[methylsilyl]bis(2-methyl-4-phenylindenyl)(2-methylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$ }hexane;
1,2-{bis[methylsilyl]bis(2-methyl-4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$ }ethane;
1,2-{bis[methylsilyl]bis(2-ethyl-4-phenylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$ }ethane;
1,2-{bis[methylsilyl]bis(2-methyl-4-naphthylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$ }ethane;
1,2-{bis[methylsilyl]bis(2-methyl-4,5-benzoidindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$ }ethane;
1,2-{bis[methylsilyl]bis(2-methyl-4-phenylindenyl)(2-methylindenyl) $Zr^+CH_2CHCHCH_2B^-(C_6F_5)_3$ }ethane.

The preparation of the novel transition metal compound of the formula I is illustrated by the following reaction schemes.

The preparation of the novel transition metal compound of the formula I is illustrated by the following reaction schemes.



L, n, M, X, B, A, R^1 and m in the formulae II, III and IV are as defined in formula I and Hal is a halogen atom such as fluorine, chlorine, bromine or iodine.

Compounds of the formula II are described in the literature (J. Okuda, Topics in Current Chemistry, Vol. 160; Springer Verlag, Berlin Heidelberg 1991, page 97). Reaction of compounds of the formula II in inert solvents with dianion compounds of the formula III, for example 1,4-butanediylolithium or 2-butene-1,4-diylmagnesium, leads to elimination of a salt and formation of the cyclic systems IV in which the M—X or the M—B bond can be a covalent bond or a coordination of the compound X—B to the metal atom M.

The compound of the formula IV can be reacted with Lewis acids of the formula AR^1_m in organic solvents, for example toluene, benzene, methylene chloride, carbon tetrachloride and petroleum spirit, to give the compound of the formula I.

The novel transition metal compounds of the formula I can be isolated or directly used for further reactions. The compounds of the formula I can also be prepared without isolation of intermediate and end stages in a single-vessel reaction from metallocene dihalides, dianion compounds and Lewis acids and be directly used for the polymerization.

Suitable solvents for this purpose are aliphatic or aromatic solvents, such as hexane or toluene, or halogenated hydrocarbons, such as methylene chloride, or halogenated aromatic hydrocarbons such as o-dichlorobenzene.

A further possibility for preparing the novel compounds of the formula I comprises the formation of metallocycles of the formula IV by electrocyclic ring-closure reaction of, for example, metallocene-bisolefin complexes or metallocene-olefin-aldehyde complexes and subsequent reaction with AR^1_m .

The present invention also relates to a process for preparing an olefin polymer by polymerization of at least one olefin in the presence of a catalyst containing at least one transition metal compound of the formula I. The polymerization can be a homopolymerization or a copolymerization.

Preference is given to polymerizing olefins of the formula $R^a-CH=CH-R^b$, where R^a and R^b are identical or different and are each a hydrogen atom, a halogen atom, an alkoxy group, a hydroxy group, an alkylhydroxy group, an aldehyde group, a carboxylic acid group or a carboxylic ester group or a saturated or unsaturated hydrocarbon radical having from 1 to 20 carbon atoms, in particular from 1 to 10 carbon atoms, which can be substituted by an alkoxy group, a hydroxy group, an alkylhydroxy group, an aldehyde group, a carboxylic acid group or a carboxylic ester group, or R^a and R^b together with the atoms connecting them can form a one or more rings. Examples of such olefins are 1-olefins such as ethylene, propylene, 1-butene, 1-hexene, 4-methyl-1-pentene, 1-octene, styrene, cyclic olefins such as norbornene, vinylnorbornene, tetracyclododecene, ethylenenorbornene, dienes such as 1,3-butadiene or 1,4-hexadiene, biscyclopentadiene or methyl methacrylate. In

particular, propylene or ethylene are homopolymerized, ethylene is copolymerized with one or more C_3-C_{20} -1-olefins, in particular propylene, and/or one or more C_4-C_{20} -dienes, in particular 1,3-butadiene, or norbornene and ethylene are copolymerized.

The polymerization is preferably carried out at a temperature of from -60 to $300^\circ C$., particularly preferably from 30 to $250^\circ C$. The pressure is from 0.5 to 2500 bar, preferably from 2 to 1500 bar. The polymerization can be carried out continuously or batchwise, in one or more stages, in solution, in suspension, in the gas phase or in a supercritical medium.

It is also possible to use mixtures of two or more transition metal compounds of the formula I. By this means, polyolefins having a broad or multimodal molecular weight distribution can be obtained.

A prepolymerization can be carried out by means of the compound of the formula I. For the prepolymerization, preference is given to using the (or one of the) olefin(s) used in the polymerization.

The compounds of the formula I can also be applied to a support, particularly for controlling the particle morphology. Suitable support materials are, for example, silica gels, aluminum oxides, solid aluminosilicates or other inorganic support materials such as, for example, magnesium chloride. Another suitable support material is a polyolefin powder in finely divided form.

The supported catalyst system can be resuspended as powder or still together with solvent and can be metered into the polymerization system as a suspension in an inert suspension medium.

To remove catalyst poisons present in the olefin, purification using an aluminum alkyl, for example trimethylaluminum, triethylaluminum or triisobutylaluminum, is advantageous. This purification can be carried out either in the polymerization system itself or the olefin is contacted with the Al compound and subsequently separated again prior to its addition to the polymerization system.

Hydrogen is added, if required, as molecular weight regulator and/or to increase the activity. The total pressure in the polymerization system is from 0.5 to 2500 bar, preferably from 2 to 1500 bar.

The compound of the formula I is here used in a concentration, based on the transition metal, of preferably from 10^{-3} to 10^{-8} , particularly preferably from 10^{-4} to 10^{-7} , mol of transition metal per dm^3 of solvent or per dm^3 of reactor volume.

If the polymerization is carried out as a suspension or solution polymerization, an inert solvent customary for the Ziegler low-pressure process is used. For example, the polymerization is carried out in an aliphatic or cycloaliphatic hydrocarbon; examples of such solvents which may be mentioned are propane, butane, hexane, heptane, isooctane, cyclohexane, methylcyclohexane. Furthermore, a petroleum or hydrogenated diesel oil fraction can be used. It is also possible to use toluene. Preference is given to carrying out the polymerization in the liquid monomer.

If inert solvents are used, the monomers are metered in gaseous or liquid form.

The duration of the polymerization can be as desired, since the catalyst system to be used according to the invention has only a small fall in polymerization activity with time.

Prior to addition of the catalyst, in particular the supported catalyst system (containing at least one novel compound of the formula I, support material and/or a polyolefin powder in

finely divided form), another aluminum alkyl compound such as, for example, trimethylaluminum, triethylaluminum, triisobutylaluminum, trioctylaluminum or isoprenylaluminum can additionally be added to the reactor to stabilize the polymerization system (for example for removing catalyst poisons present in the olefin). This is added to the polymerization system in a concentration of from 100 to 0.01 mmol of Al per kg of reactor contents. Preference is given to triisobutylaluminum and triethylaluminum in a concentration of from 10 to 0.1 mmol of Al per kg of reactor contents. This enables a small Al/M molar ratio to be selected in the synthesis of a supported catalyst system.

The novel compounds of the formula I are highly active catalyst components for olefin polymerization.

In principle, the use of cocatalysts in the polymerization reaction is not required, i.e. the novel compounds of the formula I can be used as catalyst for olefin polymerization without the need for a cocatalyst such as aluminoxane.

The following examples serve to illustrate the invention.

General procedures: Preparation and handling of organometallic compounds were carried out with exclusion of air and moisture under argon protection (Schlenk technique). All solvents required were dried prior to use by boiling for a number of hours over a suitable desiccant and subsequent distillation.

The compounds were characterized using $^1\text{H-NMR}$, $^{13}\text{C-NMR}$ and IR spectroscopy.

A. Synthesis of the Compounds of the Formula IV

The preparation of the butadiene complexes was carried out according to G. Erker, K. Engel, Ch. Sarter in R. B. King, J. J. Eisch, *Organometallic Synthesis*, Vol 3, Academic Press, New York 1986, 529:

EXAMPLE 1

Dimethylsilanediybis(2-methyl-4,5-benzoindenyl)zirconium(η^4 -butadiene)

100 ml of toluene (precooled to -40°C .) are added to a mixture of 5.0 g (8.67 mmol) of dimethylsilanediybis(2-methyl-4,5-benzoindenyl)zirconium dichloride and 2.3 g (10.4 mmol, 1.2 equivalents) of (2-butene-1,4-diyl)magnesium bistetrahydrofuran ("butadienemagnesium") which has been cooled to -40°C . While stirring vigorously, the mixture is allowed slowly to warm up to room temperature. After stirring for four hours, the dark red solution is separated via a frit from unreacted butadienemagnesium and magnesium chloride formed. The filtrate is evaporated to dryness and the residue is washed with 10 ml of pentane. This gives 4.4 g (70%) of a deep red powder.

EXAMPLE 2

Dimethylsilanediybis(2-methyl-4-phenylindenyl)zirconium(η^4 -butadiene)

100 ml of toluene (precooled to -40°C .) are added to a mixture of 5.0 g (7.95 mmol) of dimethylsilanediybis(2-methyl-4-phenylindenyl)zirconium dichloride and 2.1 g (9.5 mmol, 1.2 equivalents) of (2-butene-1,4-diyl)magnesium bistetrahydrofuran ("butadienemagnesium") which has been cooled to -40°C . While stirring vigorously, the mixture is allowed slowly to warm up to room temperature. After stirring for four hours, the dark red solution is separated via a frit from unreacted butadienemagnesium and magnesium chloride formed. The filtrate is evaporated to dryness and the residue is washed with 10 ml of pentane. This gives 3.5 g (72%) of a red-brown powder.

B. Synthesis of the Compounds of the Formula I

EXAMPLE 3

Dimethylsilanediybis(2-methyl-4,5-benzoindenyl)zirconium(η^4 -butadiene)

3.0 g (5.35 mmol) of dimethylsilanediybis(2-methyl-4,5-benzoindenyl)zirconium(η^4 -butadiene) are dissolved in 100 ml of toluene and admixed with 3.01 g (5.88 mmol, 1.1 equivalents) of tris(pentafluorophenyl)borane. The reaction solution is left stirring for 24 hours at room temperature and the strongly dark brown suspension is subsequently evaporated to half its volume. The precipitate is filtered off and washed with 10 ml of pentane. This gives 5.27 g (92%) of a sparingly soluble reddish brown powder.

EXAMPLE 4

Dimethylsilanediybis(2-methyl-4-phenylindenyl)zirconium(η^4 -butadiene)

3.0 g (4.90 mmol) of dimethylsilanediybis(2-methyl-4-phenylindenyl)zirconium(η^4 -butadiene) are dissolved in 100 ml of toluene and admixed with 2.76 g (5.39 mmol, 1.1 equivalents) of tris(pentafluorophenyl)borane. The reaction solution is left stirring for 24 hours at room temperature and the strongly dark brown suspension is subsequently evaporated to half its volume. The precipitate is filtered off and washed with 10 ml of pentane. This gives 4.84 g (88%) of a sparingly soluble reddish brown powder.

C. Polymerization Examples

EXAMPLE 5

The catalyst solution is prepared by mixing 11 mg of bis(cyclopentadienyl)zirconium(η^4 -butadiene) in 20 ml of toluene with a solution of 20.4 mg of tris(pentafluorophenyl)borane in 20 ml of toluene. 900 ml of toluene are admixed with 1 ml of a 10% strength by weight TIBA solution in toluene and subsequently with 1 ml of this catalyst solution.

For the polymerization, this solution is placed in an inert 1.5 dm³ stirred reactor, heated to 70°C . and polymerization is carried out at a pressure of 7 bar of ethylene. After 2 hours, the reactor is vented, the polymer is filtered from the suspension, washed with acetone and dried for 12 hours in a vacuum drying oven. This gives 38 g of polyethylene having an M_w of 297,000 g/mol and an M_w/M_n of 2.5 according to GPC.

EXAMPLE 6

The polymerization of Example 5 is repeated using high-purity ethylene, except that no TIBA was added. This gives 37 g of polyethylene having identical properties.

EXAMPLE 7

The polymerization of Example 5 is repeated, except that 2 ml of the catalyst solution are added and 100 ml of 1-hexene were first added to the reactor and 5 bar of ethylene were subsequently added. After 30 minutes, the reactor is vented, the polymerization is stopped using methanol and the polymer is filtered from the suspension, washed with acetone and dried for 12 hours in a vacuum drying oven. This gives 25 g of an ethylene/1-hexene copolymer containing 5.2 mol % of hexene (according to $^{13}\text{C-NMR}$) and having an M_w of 60,000 g/mol and an M_w/M_n of 2.6 according to GPC. The DSC melting point of the 2nd heating is 110°C .

EXAMPLE 8

A 1.5 dm³ autoclave, which was thoroughly flushed with ethene beforehand, is charged with 600 cm³ of an 85%

strength by weight solution of norbornene in toluene. The solution is saturated with ethene by repeated pressurization with ethene (18 bar). A suspension of 2.28 mg of 4-(η^5 -cyclopentadienyl)-4,7,7-trimethyl-(η^5 -4,5,6,7-tetrahydroindenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃ in 10 ml of toluene was added to the reactor thus prepared (in the case of hydrogen regulation, hydrogen can be injected at this point). Polymerization was carried out for one hour while stirring, with the ethene pressure being kept at 18 bar by metering in further amounts.

After the end of the reaction time, the polymerization mixture was drained into a vessel and immediately introduced into 5 dm³ of acetone, the mixture was stirred for 10 min and the precipitated product was subsequently filtered off. The filter cake was washed alternately three times each with 10% strength hydrochloric acid and acetone. It was subsequently washed to neutrality with water, the residue was slurried in acetone and filtered again. The polymer thus purified was dried at 80° C. for 15 hours in vacuo (0.2 bar). After drying, there were obtained 224 g of colorless polymer which had a glass transition temperature of 179° C., a viscosity number of 52 cm³/g, a tensile strength of 59 MPa and an elongation at break of 3.1%. The activity was 80.5 kg of polymer/hxmmol.

EXAMPLE 9

106 mg (0.385 mmol) of biscyclopentadienylzirconium (η^4 -butadiene) were dissolved in toluene and admixed with a solution of 186 mg (0.363 mmol) of B(C₆F₅)₃ in toluene. The formation of the catalyst can be recognized by the appearance of turbidity or of a precipitate. In parallel thereto, a dry 16 dm³ reactor was flushed first with nitrogen and subsequently with propylene and then charged with 10 dm³ of liquid propylene. 15 cm³ of triisobutylaluminum (20% strength in hydrocarbon, 12 mmol) were then added to the reactor and the mixture was stirred at 30° C. for 15 minutes. The catalyst suspension was subsequently added to the reactor, heated to the polymerization temperature of 70° C. (4° C./min) and the polymerization system was held for 1 hour at 70° C. by means of cooling. The polymerization was stopped by addition of 20 ml of isopropanol. The excess monomer was vented and residues of solvent were taken off in vacuo. This gave 850 g of liquid, atactic polypropylene. The catalyst activity was 8 kg of PP/(g of metallocenexh).

VN=5 cm³/g, M_w=1500 g/mol, M_w/M_n=3.2.

EXAMPLE 10

10 mg (17.9 μ mol) of rac-dimethylsilanedibis(2-methyl-4,5-benzo-1-indenyl)zirconium(η^4 -butadiene) were dissolved in 10 ml of toluene and admixed with 10 ml of a solution of 9.2 mg (18 mmol) of B(C₆F₅)₃ in toluene. The formation of the catalyst can be recognized by the appearance of turbidity or of a dark precipitate. The polymerization was carried out by a method similar to Example 9 at 70° C. The excess monomer was vented and the polymer powder was dried in vacuo. This gave 2500 g of isotactic polypropylene powder.

The catalyst activity was 250 kg of PP/(g of metallocenexh).

VN=240 cm³/g, mp.=148.7° C., M_w=298,000 g/mol, M_w/M_n=2.2, MFI_(230/2.16)=3.2 dg/min.

EXAMPLE 11

The preparation of the catalyst suspension from Example 10 was repeated, except that 3 mg (4.8 μ mol) of rac-

dimethylsilanedibis(2-methyl-4-phenyl-1-indenyl)zirconium(η^4 -butadiene) dissolved in 10 cm³ of toluene were reacted with 2.5 mg (4.9 μ mol) of B(C₆F₅)₃ dissolved in 10 cm³ of toluene. The polymerization was carried out at 60° C. after adding the catalyst suspension to the reactor. The polymerization gave 2250 g of isotactic polypropylene powder.

The catalyst activity was 750 kg of PP/(g of metallocenexh).

VN=620 cm³/g, mp.=155° C., MFI_(230/5)=0.35 dg/min.

EXAMPLE 12

The preparation of the catalyst suspension from Example 10 was repeated, except that 10 mg (21 μ mol) of rac-dimethylsilanedibis(2-methyl-1-indenyl)zirconium(η^4 -butadiene) dissolved in 10 cm³ of toluene were reacted with 10.7 mg (21 μ mol) of B(C₆F₅)₃ dissolved in 10 cm³ of toluene. The polymerization gave 1900 g of isotactic polypropylene powder. The catalyst activity was 190 kg of PP/(g of metallocenexh).

VN=180 cm³/g, mp.=145° C., M_w=192,000, M_w/M_n=2.2, MFI_(230/2.16)=12 dg/min.

EXAMPLE 13

The preparation of the catalyst suspension from Example 10 was repeated, except that 10 mg (20.2 μ mol) of phenylmethylmethylenefluorenylcyclopentadienylzirconium-(η^4 -butadiene) dissolved in 10 cm³ of toluene were reacted with 10.7 mg (21 μ mol) of B(C₆F₅)₃ dissolved in 10 cm³ of toluene. The polymerization gave 1100 g of syndiotactic polypropylene powder.

The catalyst activity was 110 kg of PP/(g of metallocenexh).

VN=137 cm³/g, mp.=133° C., M_w=122,000 g/mol, M_w/M_n=2.3.

EXAMPLE 14

Reactor Preparation

A 1500 ml reactor which had been repeatedly flushed with nitrogen was charged with 1000 ml of an 85% strength by weight solution of norbornene in toluene and the solution was heated to 70° C. The solution was saturated with ethylene by repeated pressurization with ethylene (16 bar gauge pressure). 2 ml of a 20% strength triethylaluminum solution in toluene were added to the depressurized reactor in a countercurrent of ethylene and the mixture was subsequently stirred for 15 minutes.

Catalyst Preparation

A solution of 12.6 mg of tris(pentafluorophenyl)borane (0.025 mmol) in 1.26 ml of toluene was added to the solution of 9.0 mg of (butadiene)isopropylene(1-indenyl)cyclopentadienylzirconium (0.025 mmol) in 0.9 ml of toluene. The catalyst mixture was preactivated for 25 minutes at room temperature.

Polymerization and Isolation

The catalyst mixture was added to the prepared reaction solution and an ethylene pressure of 16 bar was subsequently applied as quickly as possible. Polymerization was carried out for 2 hours at 70° C. while stirring at about 750 rpm, with the ethylene pressure being kept constant at 16 bar.

To end the reaction, the reactor was first vented and the reaction solution was subsequently drained into a vessel. The polymer was precipitated in 2500 ml of acetone and filtered after stirring for 5 minutes. The filter cake was repeatedly washed alternately with 10% strength hydrochloric

ric acid and acetone. It was subsequently washed to neutrality with water and, after addition of 1000 ml of acetone, filtered. The powder thus purified was dried for 15 hours at 80° C. at a pressure of 0.2 bar.

Characterization

After drying, 30 g of colorless powder were obtained; this corresponds to an activity of 610 g of polymer/hxmmol of metallocene. A viscosity number of 106 cm³/g and a glass transition temperature of 135° C. were measured on the polymer. No melting point was able to be detected by means of thermal analysis.

EXAMPLE 15

30 mg (31 μmol) of *rac*-dimethylsilanediylbis(2-methyl-1-indenyl)Zr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃ are dissolved in 30 ml of toluene. 10 g of SiO₂ are stirred into the catalyst solution until a homogeneous distribution is achieved.

The solid is then filtered off from the solvent and washed twice with 10 ml of toluene.

In parallel thereto, a dry 16 dm³ reactor was flushed first with nitrogen and subsequently with propylene and charged with 10 dm³ of liquid propylene. 15 cm³ of triisobutylaluminum (20% strength in hydrocarbon, 12 mmol) were then added to the reactor and the mixture was stirred at 30° C. for 15 minutes. The catalyst suspension was subsequently added to the reactor, heated to the polymerization temperature of 70° C. (4° C./min) and the polymerization system was held at 70° C. for 1 hour by cooling. The polymerization was stopped by addition of 20 ml of isopropanol. The excess monomer was vented and solvent residues were taken off in vacuo.

The polymerization gives 2.5 kg of isotactic polypropylene powder. The catalyst activity was 83 kg of PP/(g of metallocenexh).

VN=184 cm³/g, mp.=145° C., M_w=193,000 g/mol, M_w/M_n=2.2.

The reactor shows no deposits on walls or stirrer.

EXAMPLE 16

a) Preparation of the Catalyst Component

A solution of 1 μmol of biscyclopentadienylzirconium (η⁴-butadiene) in 1 ml of toluene is admixed with a solution of 1 μmol of tris(pentafluorophenyl)borane in 10 ml of toluene and, after a reaction time of 15 minutes, evaporated in vacuo to a volume of 2 ml. In parallel thereto, 4 g of Accurel LDPE powder in a sieve fraction of smaller than 200 μm are dried in vacuo and flushed with argon. The support powder is stirred into the catalyst solution until a homogeneous distribution is achieved.

b) Polymerization

A dry 1.5 dm³ stirred reactor is flushed with nitrogen to remove the oxygen and charged with 0.9 dm³ of an inert diesel oil (bp. from 100 to 120° C.). After flushing with ethylene, it is heated to 70° C. and the catalyst is added as powder. Polymerization is subsequently carried out without additional activator at a pressure of 7 bar of ethylene. After 1 hour, the reactor is vented, the polymer is filtered from the suspension and dried for 12 hours in a vacuum drying oven. This gives 18 g of polyethylene powder having a bulk density of 0.253 kg/dm³ and a viscosity number VN of 389 cm³/g. The polydispersity M_w/M_n is 2.6 (according to GPC). The reactor shows no deposits on walls or stirrer.

EXAMPLE 17

a) Preparation of the Catalyst Component

BiscyclopentadienylZr⁺CH₂CHCHCH₂B⁻(C₆F₅)₃ was supported on SiO₂ using a method similar to Example 15.

b) Gas-Phase Polymerization of Ethylene

A gas-phase polymerization of ethylene was carried out in a 2 dm³ steel autoclave having polished walls. The fluidized bed was generated mechanically by means of a double-helix stirrer going around the wall, using an initial charge of 10 g of polyethylene powder as seed bed. Via a pressure burette, first the cocatalyst (2 mmol) of triisobutylaluminum in 2 cm³ of isopentane and subsequently 1 g of the catalyst mixture (19.2 μmol of Zr) were metered in. The polymerization was subsequently carried out at 8 bar partial pressure of ethylene at a temperature of 80° C. for 1 hour and ended by venting the autoclave.

This gave 118 g of polyethylene having a VN of 309 ml/g, corresponding to an activity of 6.2 kg of PE/mmol of metallocene.

EXAMPLE 18

The preparation of the catalyst suspension of Example 10 was repeated, except that 10 mg (24 μmol) of dimethylmethylene-9-fluorenylcyclopentadienylzirconium (4-butadiene) dissolved in 10 cm³ of toluene were reacted with 12.8 mg (25 μmol) of B(C₆F₅)₃ dissolved in 10 cm³ of toluene. The polymerization was carried out after metering the catalyst suspension into the reactor at 60° C. The polymerization gave 900 g of syndiotactic polypropylene powder. The catalyst activity was 90 kg of PP/(g of metallocenexh).

VN=92 cm³/g, m.p.=126° C., M_w=63,000 g/mol, M_w/M_n=2.1

EXAMPLE 19

The preparation of the catalyst suspension of Example 10 was repeated, except that 5 mg (8 μmol) of *rac*-dimethylsilanediylbis(2-methyl-4,6-diisopropyl-1-indenyl) zirconium(4-butadiene) dissolved in 10 cm³ of toluene were reacted with 4.1 mg (8.1 μmol) of B(C₆F₅)₃ dissolved in 10 cm³ of toluene. The polymerization was carried out after metering the catalyst suspension into the reactor at 60° C. The polymerization gave 2100 g of isotactic polypropylene powder.

The catalyst activity was 420 kg of PP/(g of metallocenexh).

VN=423 cm³/g, mp.=154° C., MFI_(230/5)=3.1 dg/min, M_w=588,000 g/mol, M_w/M_n=3.5.

EXAMPLE 20

The preparation of the catalyst suspension of Example 11 was repeated. The polymerization was carried out after metering the catalyst suspension into the reactor at 70° C. The polymerization gave 2800 g of isotactic polypropylene powder.

The catalyst activity was 933 kg of PP/(g of metallocenexh).

VN=544 cm³/g, mp.=154° C., MFI_(230/5)=1.3 dg/min, M_w=741,000 g/mol, M_w/M_n=2.8.

EXAMPLE 21

The preparation of the catalyst suspension of Example 12 was repeated, except that the 16 dm³ reactor was charged